

Mutual Solubilities of Some Hydrocarbon Oils and Liquid Ammonia. I. Solubility Data

By Kiyoharu ISHIDA

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Liquid ammonia has good solvency and selectivity for the extraction of aromatic hydrocarbons^{1,2}, olefinic hydrocarbons^{1,2} or phenols³ from hydrocarbon mixtures, and there is a possibility of the use of liquid ammonia as a solvent for the separation of hydrocarbons. It is desirable to have at hand accurate liquid-equilibrium data in order that the relative value of various solvents can be compared. However, relatively few ternary systems containing liquid ammonia have been investigated. Moreover, even for the binary systems, only a few solubility data of hydrocarbon oils and liquid ammonia have been reported^{2,4-6}. When data on the mutual solubilities are available, it is possible to predict the equilibrium relations for the ternary system from the mutual solubilities between solvent and each of two components⁷.

The paucity of information about the liquid equilibrium data for hydrocarbons and liquid ammonia prompted the author to obtain the knowledge of quantitative solubility relations. This paper includes solubility data for the representative compounds of olefins and saturated hydrocarbons at around room temperature, and those for aromatics at the temperatures near the critical solution temperature. As representative compounds of hydrocarbons, those in the C₇ to C₉ range for aromatics and in the C₆ to C₈ range for olefins and saturated hydrocarbons were mainly selected.

Experimental Procedure and Materials

Solubilities were determined by the same

method as described in the previous paper^{8,9}. Cloud points could be determined to within $\pm 0.05^\circ\text{C}$ or better by using the thermometer which was graduated in tenths of a degree and corrected by the P. T. R. thermometer. Mutual solubilities at the temperatures far from the critical solution temperature were obtained by determining the composition of the two liquid phases in equilibrium at a given temperature ($\pm 0.05^\circ\text{C}$). About five grams ($\pm 0.0005\text{ g}$) of each of the separate phases were used for the analysis at each time, and the concentration of ammonia was determined by titrating with 0.5 N sodium hydroxide solution the excess of sulfuric acid which absorbed all ammonia in the liquid phase. The determination was repeated several times for each phase at a given temperature, and averaged. The average error was less than 0.1% with a maximum error of 0.4%.

Except for some of the materials, which were commercially available products purified by the ordinary methods, many hydrocarbons used for the determination were synthesized and carefully purified. In Table 1, their physical constants are listed together with the values in the literature¹⁰.

n-Hexane and *n*-octane were synthesized from corresponding alkyl bromides according to Wurtz's method. Propylbenzene was prepared from bromobenzene and propyl bromide by Fittig reaction. *iso*-Propylbenzene was synthesized according to H. Meyer et al.¹⁰. *o*-Xylene was prepared by the condensation of *o*-bromotoluene, which was synthesized by means of Sandmeyer reaction from acet-*o*-toluide of melting point 110°C as a starting material and methyl iodide using metallic sodium and purified by careful distillation. *m*-Xylene was obtained by decomposing *m*-xylene sulfonate of melting point 60°C which was prepared and purified from a commercial product by removing the *p*-isomer according to Clark et al.¹⁵ after the sulfonation and the decomposition were repeated. *p*-Xylene was prepared by reducing *p*-chloromethyltoluene obtained by chloro-

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TABLE I
 PHYSICAL PROPERTIES OF HYDROCARBONS USED FOR THE DETERMINATIONS

| Name | b. p., °C | | d_4^{20} | | n_D^{20} | | Remarks |
|---------------------------|-----------|---------------------|------------|---------------------|------------|---------------------|--|
| | Obs. | Lit. ¹⁰⁾ | Obs. | Lit. ¹⁰⁾ | Obs. | Lit. ¹⁰⁾ | |
| <i>n</i> -Hexane | 68.7 | 68.740 | 0.6594 | 0.65937 | 1.3749 | 1.37486 | a |
| <i>n</i> -Heptane | 98.3 | 98.427 | 0.6838 | 0.68376 | 1.3878 | 1.38764 | b ^{8,9)} |
| <i>n</i> -Octane | 125.4 | 125.665 | 0.7026 | 0.70252 | 1.3976 | 1.39743 | a |
| 2,2,4-Trimethylpentane | 99.2 | 99.238 | 0.6919 | 0.69192 | 1.3916 | 1.39145 | b |
| <i>n</i> -Cetane | 286.6 | 286.793 | 0.7749 | 0.77344 | 1.4350 | 1.43453 | c, m. p. 17.2 Lit. 18.165 |
| Cyclohexane | 80.5-81.0 | 80.738 | 0.7788 | 0.77855 | 1.4263 | 1.42623 | d ¹¹⁾ , m. p. 6.32 Lit. 6.554 |
| Methylcyclohexane | 100.9 | 100.934 | 0.7686 | 0.76939 | 1.4231 | 1.42312 | c |
| Decalin <i>cis</i> | 189-190 | 195.69 | 0.8859 | 0.8965 | 1.4750 | 1.4810 | c ¹²⁾ |
| Decalin <i>trans</i> | | 187.25 | | 0.8699 | | 1.4695 | |
| Cyclohexene | 82.8 | 82.979 | 0.8096 | 0.81096 | 1.4465 | 1.44654 | c, Br. No. 194.6 Theor. 194.58 |
| 1-Octene | 122.6 | 121.280 | 0.7161 | 0.71492 | 1.4086 | 1.40870 | a ¹¹⁾ , Br. No. 142.2 Theor. 142.7 |
| Styrene | 48/24.1 | 145.2 | 0.9059 | 0.90600 | 1.5468 | 1.54682 | c ¹⁾ , Br. No. 151.2 Theor. 153.5 |
| Toluene | 110.5 | 110.625 | 0.8660 | 0.86694 | 1.4961 | 1.49693 | c ^{8,9)} |
| Ethylbenzene | 136.0 | 136.186 | 0.8670 | 0.86702 | 1.4959 | 1.49588 | a ¹⁾ |
| <i>o</i> -Xylene | 144.2 | 144.414 | 0.8805 | 0.88020 | 1.5045 | 1.50545 | a, m. p. -25.3 Lit. -25.182 |
| <i>m</i> -Xylene | 139.1 | 139.103 | 0.8636 | 0.86417 | 1.4971 | 1.49722 | d, m. p. -47.9 Lit. -47.872 |
| <i>p</i> -Xylene | 138.4 | 138.351 | 0.8605 | 0.86105 | 1.4957 | 1.49582 | a, m. p. 13.2 Lit. 13.263 |
| Propylbenzene | 159.2 | 159.217 | 0.8619 | 0.86204 | 1.4920 | 1.49202 | a |
| <i>iso</i> -Propylbenzene | 152.4 | 152.392 | 0.8618 | 0.86179 | 1.4912 | 1.49145 | a ¹³⁾ |
| Mesitylene | 164.7 | 164.715 | 0.8647 | 0.86518 | 1.4993 | 1.49937 | a ¹⁴⁾ |
| 1-Methylnaphthalene | 244.4 | 244.642 | 1.0200 | 1.02015 | 1.6174 | 1.6174 | a |
| Tetralin | 207 | 207.57 | 0.9702 | 0.9702 | 1.5414 | 1.54135 | d ¹²⁾ |

a) This material was synthesized.

b) This material is the reference fuel for Octane Number determination.

c) Commercially available product was purified according to the ordinary method.

d) Commercially available product was purified according to the description in the literature.

methylation of toluene, and purified by the conversion in to the sulfonate which melted at 86°C after three recrystallizations from water.

Mesitylene was synthesized by sulfuric acid condensation of acetone¹⁴⁾. 1-Methylnaphthalene was synthesized by the reduction of 1-chloromethylnaphthalene which was obtained by the chloromethylation of naphthalene, and purified by applying chromatographic cleavage of the picrate whose melting point was 141-141.5°C. Methods of purifying for the other materials have been described in the previous paper^{8,11,12)}.

Results

Mutual solubility data of liquid ammonia and paraffins, naphthenes and olefins are given in Table II.

Values for *n*-heptane⁹⁾, cyclohexane¹⁾, decalin¹²⁾ and purified commercial hexane which is used for the extraction of vegetable oils^{1,11)} are also given in Table II

for convenience of comparison.

As will be clear from Table II, it is observed for liquid ammonia-saturated hydrocarbons systems that within the experimental range, naphthenic hydrocarbons are more soluble in liquid ammonia at a given temperature than paraffins which have the same number of carbon atoms, whereas the quantities of ammonia dissolved in hydrocarbon rich phase are greater in paraffins; it is also observed that solubilities decrease as the molecular weight increases. For binary systems of aliphatic hydrocarbons and liquid ammonia, it is observed that logarithms of solubilities of paraffins in each phase are almost proportional to those of vapor pressures of these hydrocarbons at a given temperature, and that their solubilities are small compared with those of olefins.

The experimental data for aromatic

TABLE II
MUTUAL SOLUBILITY DATA FOR PARAFFINS, NAPHTHENES AND OLEFINS WITH
LIQUID AMMONIA, Wt. % OF NH_3

| Material | Phase | Temperature, °C | | | | | |
|---|------------------|--|---------------------------------------|---------------------------------------|---------------------------------------|---------------------------------------|---------------------------------------|
| | | 30 | 20 | 10 | 0 | -7.5 | -15 |
| Purified Hexane Used for Vegetable Oil Extraction | {Upper {Lower | | 94.4 6.1 | | | | |
| <i>n</i> -Hexane | {Upper {Lower | | 94.9 ₄ 5.7 ₈ | | 97.4 ₁ 3.0 ₂ | | |
| <i>n</i> -Heptane | {Upper {Lower | | 96.9 ₂ 4.8 ₅ | | 98.1 ₆ 2.7 ₃ | 98.4 ₉ 2.2 ₃ | 98.8 ₀ 1.7 ₁ |
| <i>n</i> -Octane | {Upper {Lower | | 97.7 ₅ 4.1 ₃ | | 98.5 ₈ 2.2 ₉ | | |
| 2,2,4-Trimethylpentane | {Upper {Lower | | 96.8 ₉ 5.0 ₈ | | 98.5 ₁ 2.7 ₃ | | |
| <i>n</i> -Cetane | {Upper {Lower | 98.5 ₇ 3.0 ₈ | 99.4 ₄ 2.4 ₃ | | | | |
| Cyclohexane | {Upper {Lower | | 94.2 ₂ 3.9 ₉ | | 96.7 ₃ 2.1 ₂ | | |
| Methylcyclohexane | {Upper {Lower | | 94.7 ₂ 4.1 ₅ | | 97.8 ₃ 2.2 ₀ | | |
| Decalin | {Upper {Lower | | 97.8 ₄ 2.2 ₈ | | 98.3 ₅ 1.4 ₀ | | |
| 1-Octene | {Upper {Lower | | 93.6 ₉ 7.8 ₈ | | 96.8 ₃ 4.0 ₉ | | |
| Cyclohexene | {Upper {Lower | 72.6 ₄ 15.2 ₂ | 82.1 ₉ 9.3 ₉ | 88.0 ₀ 6.3 ₇ | 91.6 ₁ 4.5 ₅ | | |

TABLE III
SOLUBILITY OF AROMATICS IN LIQUID AMMONIA, Wt. % of NH_3

| Material | Temperature, °C | | | | | | | | |
|-------------------------------------|-------------------|-------------------|-------------------|-------------------|-------------------|-------------------|-------------------|-------------------|-------------------|
| | 30 | 25 | 20 | 15 | 10 | 5 | 0 | -5 | -15.5 |
| Ethylbenzene | | miscible | | | 57.0 ₁ | 71.4 ₇ | 78.1 ₁ | 82.2 ₅ | 87.0 ₂ |
| <i>o</i> -Xylene | | miscible | | | 61.8 ₃ | 72.6 ₃ | 78.8 ₂ | 82.9 ₆ | |
| <i>m</i> -Xylene | | miscible | | | 69.5 ₀ | 76.7 ₂ | 81.0 ₂ | 84.2 ₀ | |
| <i>p</i> -Xylene | | miscible | | | 64.9 ₂ | 74.4 ₇ | 79.9 ₄ | 83.7 ₅ | |
| Propylbenzene | miscible | | 68.5 ₀ | 77.3 ₅ | 82.8 ₂ | 86.4 ₆ | 88.8 ₉ | | |
| <i>iso</i> -Propylbenzene | miscible | | C.S.T. | 70.8 ₂ | 78.9 ₂ | 83.3 ₁ | 86.7 ₂ | | |
| Mesitylene | 67.6 ₇ | 76.2 ₀ | 81.0 ₉ | 84.8 ₅ | 87.5 ₇ | 89.9 ₂ | 91.4 ₄ | | |
| 1-Methylnaphthalene | | 64.3 ₇ | 71.7 ₈ | 77.1 ₆ | 81.1 ₂ | 83.9 ₄ | 85.9 ₄ | | |
| Tetralin | | | 86.3 ₉ | | | | 93.7 ₂ | | |
| Temperature, °C ($\pm 0.1^\circ$) | | -10 | | -15 | | -20 | | -25 | |
| Material | | | | | | | | | |
| Toluene | | 64.4 ₄ | | 73.1 ₈ | | 78.5 ₉ | | | |
| Styrene | | | | | 68.7 ₆ | | 76.3 ₄ | | 79.8 ₃ |

hydrocarbons are given in Tables III and IV. *p*-Xylene is present as crystals at the experimental temperatures, but the mixture with liquid ammonia was liquid over the experimental temperature range above 5°C. *p*-Xylene-rich layer stayed in a supercooled liquid state at the temperatures of 0° and -5°C, and it was difficult to cause it to crystallize by mere agitation. Occasionally, *p*-xylene-rich layer was caused to crystallize by the stimulation such as the release of a portion of the solution from the bottle containing the system, which closed the reducing valve and made it

impossible to continue the experiment. The data for *p*-xylene at the temperatures of 0° and -5°C given in Table IV are values in a supercooled condition. In Tables III and IV, the data for tetralin¹²⁾ and toluene⁹⁾ are also adopted for comparison from the previous paper.

In Table V are given the results of the determinations of compositions and cloud points for the binary systems of aromatics and liquid ammonia at temperatures near the critical solution temperature. The critical solution temperatures and their compositions estimated graphically from

TABLE IV
SOLUBILITY OF LIQUID AMMONIA IN AROMATIC HYDROCARBONS, Wt. % OF NH₃
Temperature, °C

| Material | 30 | 25 | 20 | 15 | 10 | 5 | 0 | -5 | -15.5 |
|---------------------------|-------------------|-------------------|-------------------|-------------------|-------------------|-------------------|-------------------|-------------------|------------------|
| Ethylbenzene | | miscible | | | 30.7 ₆ | 18.9 ₀ | 14.1 ₃ | 11.3 ₁ | 8.0 ₀ |
| <i>o</i> -Xylene | | miscible | | | 24.3 ₂ | 16.9 ₅ | 13.0 ₇ | 10.8 ₃ | |
| <i>m</i> -Xylene | | miscible | | | 20.2 ₅ | 15.0 ₃ | 11.8 ₇ | 9.6 ₇ | |
| <i>p</i> -Xylene | | miscible | | | 22.1 ₃ | 16.1 ₂ | 12.7 ₉ | 10.3 ₃ | |
| Propylbenzene | miscible | | 22.5 ₄ | 16.5 ₅ | 13.1 ₇ | 10.8 ₉ | 9.1 ₅ | | |
| <i>iso</i> -Propylbenzene | miscible | | C.S.T. | 20.5 ₇ | 15.2 ₆ | 12.2 ₃ | 10.0 ₁ | | |
| Mesitylene | 21.0 ₄ | 15.5 ₂ | 12.5 ₇ | 10.3 ₆ | 8.6 ₂ | 7.2 ₆ | 6.2 ₉ | | |
| 1-Methylnaphthalene | | 22.2 ₄ | 17.3 ₆ | 14.3 ₀ | 12.1 ₉ | 10.4 ₃ | 9.1 ₂ | | |
| Tetralin | | | 8.0 ₉ | | | | 4.7 ₁ | | |
| Temperature, °C (±0.1°) | | -10 | | -15 | -20 | -25 | -30 | | |
| Material | | | | | | | | | |
| Toluene | | 20.2 ₂ | | 15.3 ₄ | 12.4 ₁ | | | | |
| Styrene | | | | | 20.7 ₅ | 14.6 ₆ | 11.9 ₅ | | |

TABLE V
CLOUD POINTS AND THEIR COMPOSITION FOR AROMATICS WITH LIQUID AMMONIA
Cloud Pt., °C NH₃ Wt. % Cloud Pt., °C NH₃ Wt. % Cloud Pt., °C NH₃ Wt. %

| Styrene | | <i>o</i> -Xylene | | <i>p</i> -Xylene | |
|---------------------------|-------------------|-------------------|-------------------|---------------------|-------------------|
| -16.8 | 27.6 ₅ | 11.5 | 34.3 ₃ | 12.3 | 29.9 ₃ |
| -16.3 | 30.2 ₅ | 11.9 | 41.9 ₇ | 12.8 | 42.9 ₀ |
| -15.85 | 32.1 ₁ | 11.9 | 45.3 ₄ | 12.6 | 48.0 ₉ |
| -15.7 | 34.7 ₁ | 11.8 | 47.9 ₃ | 12.6 | 48.2 ₂ |
| -15.5 | 40.3 ₃ | 11.5 | 54.5 ₅ | 12.5 | 52.0 ₀ |
| -15.5 | 42.4 ₄ | 11.3 | 56.6 ₈ | 11.7 | 58.0 ₃ |
| -15.5 | 43.9 ₁ | 11.2 | 57.0 ₆ | 11.6 | 58.9 ₉ |
| -15.8 | 50.2 ₂ | 11.1 | 57.6 ₂ | 10.2 | 64.0 ₉ |
| -17.8 | 62.5 ₃ | 10.6 | 60.2 ₆ | 12.8* | 40.5** |
| -15.5* | 43.9** | 11.9* | 43.3** | | |
| Ethylbenzene | | <i>m</i> -Xylene | | Propylbenzene | |
| 9.0 | 26.2 ₁ | 14.1 | 31.6 ₃ | 21.3 | 24.9 ₃ |
| 10.2 | 32.1 ₁ | 14.6 | 42.1 ₀ | 23.6 | 36.0 ₄ |
| 10.5 | 36.0 ₇ | 14.4 | 46.5 ₁ | 23.9 | 40.2 ₃ |
| 10.6 | 37.2 ₂ | 13.9 | 54.0 ₉ | 23.9 | 41.8 ₇ |
| 10.7 | 44.2 ₄ | 13.8 | 54.9 ₄ | 23.0 ₅ | 56.7 ₄ |
| 10.4 | 51.7 ₇ | 13.5 | 56.7 ₅ | 22.6 | 58.8 ₅ |
| 10.1 | 55.4 ₄ | 11.6 | 65.0 ₇ | 22.4 ₃ | 59.5 ₉ |
| 0.0 | 62.2 ₀ | 14.6* | 41.5** | 23.9* | 44.7** |
| 10.7* | 43.4** | | | | |
| <i>iso</i> -Propylbenzene | | Mesitylene | | 1-Methylnaphthalene | |
| 18.0 | 25.2 ₇ | 32.6 | 26.8 ₂ | 26.0 | 23.7 ₃ |
| 19.0 ₅ | 28.5 ₀ | 33.8 | 36.5 ₁ | 27.4 | 27.4 ₁ |
| 19.8 | 34.2 ₃ | 33.9 | 39.6 ₂ | 27.4 ₅ | 27.4 ₃ |
| 20.0 | 42.5 ₇ | 33.9 | 41.8 ₃ | 28.6 | 36.1 ₇ |
| 19.9 | 48.5 ₈ | 33.9 | 45.0 ₂ | 28.8 | 42.3 ₄ |
| 19.7 | 52.7 ₄ | 33.9 | 45.4 ₇ | 28.8 | 44.4 ₇ |
| 19.6 | 54.3 ₄ | 33.8 ₅ | 48.7 ₂ | 28.7 ₅ | 47.6 ₇ |
| 19.3 | 56.7 ₅ | 33.7 | 52.7 ₈ | 28.7 | 48.8 ₃ |
| 18.0 | 63.7 ₅ | 33.6 | 53.0 ₇ | 28.5 | 50.9 ₈ |
| 20.0* | 71.7** | 33.5 ₅ | 53.6 ₁ | 28.2 | 53.5 ₂ |
| | | 32.9 | 59.5 ₆ | 27.0 | 59.2 ₆ |
| | | 32.4 ₅ | 61.1 ₈ | 28.8* | 42.6** |
| | | 33.9* | 42.9** | | |

* Critical solution Temperature.

** Critical Composition.

the data given in Tables III, IV and V are also given in Table V.

The critical solution temperatures for toluene⁹) and *iso*-propylbenzene with liquid ammonia in the present investigation, -7.4° and 20.0°C , are lower than those given in the literature⁶), -5° and 25°C , respectively. But, the value for *m*-xylene, 14.6°C , agrees with that obtained by Kraus, et al.⁴), 14.7°C , which is believed to be accurate. The critical composition for this system is 81.5 mole per cent. of ammonia and compared with the Kraus' value of 81.4 mole per cent. ammonia. The critical solution temperature for 1-methylnaphthalene with liquid ammonia is 28.8°C by the present determination, compared with the Francis' value of 28°C ⁶).

In the case of all these systems, it will be clear from Tables II, III and IV that solubilities in both phases are smaller at lower temperatures exhibiting positive deviations from Raoult's law, and roughly symmetrical on the basis of weight fraction. However, as the molecular weight of ammonia is considerably small compared with that of any other component, the solubility curves lean to the ammonia side on the basis of mole fraction expressing unsymmetrical form, as shown in Fig. 1. The mole fractions of ammonia in hydrocarbon-rich phase are greater than those of oils in liquid ammonia rich phase. Solubilities of these hydrocarbons in liquid ammonia are less than 10 mole per cent., except for the cases in the neighborhood of the critical solution temperature, and the solubility change in ammonia-rich phase due to temperature variation is small compared with that in the hydrocarbon-rich phase.

In Fig. 1, in addition to the mutual solubilities of aromatic hydrocarbons and liquid ammonia, the concentrations of ammonia in hydrocarbon-rich phase for other representative hydrocarbons are shown on the basis of mole fraction. The values of Kraus, et al. for *m*-xylene are also given for comparison. Solubility curves for paraffins, naphthenes and olefins in liquid ammonia-rich phase are omitted in the figure except for *n*-heptane, because they are so nearly of the same order that the curves for them can not be expressed clearly without overlapping.

Summary

In order to obtain the quantitative knowledge on the solubility relations for

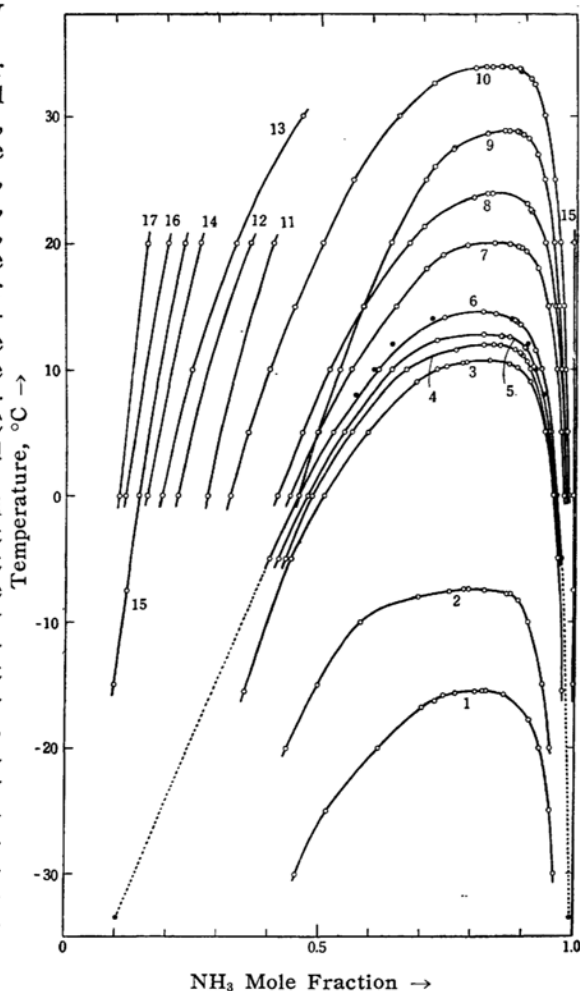


Fig. 1. Solubility curves for some hydrocarbons and liquid ammonia.

1. Styrene
2. Toluene
3. Ethylbenzene
4. *o*-Xylene
5. *p*-Xylene
6. *m*-Xylene (• Kraus value)
7. *iso*-Propylbenzene
8. Propylbenzene
9. 1-Methylnaphthalene
10. Mesitylene
11. Tetralin
12. 1-Octene
13. Cyclohexene
14. 2,2,4-Trimethylpentane
15. *n*-Heptane
16. Methylcyclohexane
17. Decalin

liquid ammonia systems, mutual solubilities of aromatic hydrocarbons and liquid ammonia were determined at the several temperatures near the critical

solution temperature, and data for other hydrocarbons were mainly obtained at 20° and 0°C. These results were presented in tables and a figure.

*The Chemical Research
Institute of Non-Aqueous Solutions
Tohoku University
Katabira-cho, Sendai*